

# 第三章 多组分系统的热力学，逸度和活度

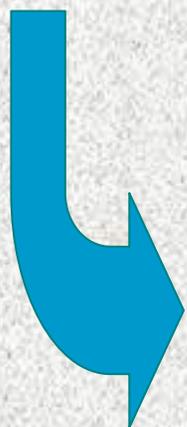
物理化学多媒体课堂教学软件 V1.0版

# 3-1 引言

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# 基本术语

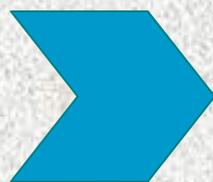
**混合物** 含有一种以上物质的**均相**系统，其中任何部分都具有相同的性质。



气态混合物

液态混合物

固态混合物



流体混合物

# 基本术语

**溶液** 含有一种以上物质的均相系统，其中一种或数种物质称为**溶剂**，其它的称为**溶质**，溶质溶解于溶剂中形成溶液。



气态溶液

液态溶液

固态溶液



稀溶液

# 组成表示方法

## (1) 物质B的摩尔分数

——B物质的量与混合物(或溶液)的总量之比。

$$x_B (y_B) \stackrel{\text{def}}{=} \frac{n_B}{n}$$

$$n = \sum_B n_B = n_{B_1} + n_{B_2} + \cdots + n_{B_K}$$

$$\sum_B x_B (y_B) = x_{B_1} + x_{B_2} + \cdots + x_{B_K} = 1$$

# 组成表示方法

## (2)物质B的质量分数

——B物质的质量与混合物(或溶液)的质量之比。

$$w_B \stackrel{\text{def}}{=} \frac{m_B}{\sum_{B'} m_{B'}} \stackrel{\text{def}}{=} \frac{n_B M_B}{\sum_{B'} n_{B'} M_{B'}}$$

$$\sum_B w_B = w_{B_1} + w_{B_2} + \cdots + w_{B_K} = 1$$

# 组成表示方法

## (3) 物质B的体积分数

$$\varphi_B \stackrel{\text{def}}{=} \frac{n_B V_B^*}{\sum_{B'} (n_{B'} V_{B'}^*)}$$

$$\sum_B \varphi_B = \varphi_{B_1} + \varphi_{B_2} + \cdots + \varphi_{B_K} = 1$$

# 组成表示方法

## (4)物质B的质量摩尔浓度

——溶液中溶质B的物质的量除以溶剂A的质量。

$$b_B(m_B) \stackrel{\text{def}}{=} \frac{n_B}{\sum_A (n_A M_A)}$$

——常用单位： $\text{mol} \cdot \text{kg}^{-1}$

## 组成表示方法

### (5)物质B的浓度(物质的量浓度)

——溶液中溶质B的物质的量除以溶液的体积。

$$c_B([\text{B}]) \stackrel{\text{def}}{=} \frac{n_B}{V}$$

——常用单位:  $\text{mol} \cdot \text{m}^{-3}$

# 不同组成表示方法之间相互换算

设二元系(A, B)

$$\begin{aligned}x_B &= \frac{M_A w_B}{M_B w_A + M_A w_B} = \frac{V_A^* \varphi_B}{V_B^* \varphi_A + V_A^* \varphi_B} \\ &= \frac{M_A b_B}{M_A b_B + 1} = \frac{M_A c_B}{M_A c_B + \rho - c_B M_B}\end{aligned}$$

—— $\rho$  是溶液的密度  $\text{kg} \cdot \text{m}^{-3}$

## 本章框架

### ◆ 多组分系统的热力学基本方程

偏摩尔量

组成可变的多元系的热力学基本方程

主要应用：

### ◆ 多组分系统物质特性的描述

逸度、活度和混合性质

# 3-2 偏摩尔量

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# 1. 偏摩尔量的定义与物理意义

设广延性质  $X$ ，由状态函数的基本假定

$$X = X(T, p, n_1, n_2, \dots, n_K)$$

$$dX = \left( \frac{\partial X}{\partial T} \right)_{p, n_j} dT + \left( \frac{\partial X}{\partial p} \right)_{T, n_j} dp + \sum_{i=1}^K \left( \frac{\partial X}{\partial n_i} \right)_{T, p, n_{j \neq i}} dn_i$$

偏摩尔量

$$X_i \stackrel{\text{def}}{=} \left( \frac{\partial X}{\partial n_i} \right)_{T, p, n_{j \neq i}}$$

$$dX = \left( \frac{\partial X}{\partial T} \right)_{p, n_j} dT + \left( \frac{\partial X}{\partial p} \right)_{T, n_j} dp + \sum_{i=1}^K X_i dn_i$$

$$X_i \stackrel{\text{def}}{=} \left( \frac{\partial X}{\partial n_i} \right)_{T, p, n_{j \neq i}}$$

$X_i$  是状态函数，强度性质

$$X_i = X_i(T, p, x_1, x_2, \dots, x_{K-1})$$

$X_i$  是在系统恒定  $T$ ,  $p$  和其它物质的量时，改变  $1\text{mol } i$  物质引起的系统广延性质  $X$  的变化。

对纯组分系统  $X_i$  即  $X_i^*$

# 偏摩尔量与摩尔量的区别

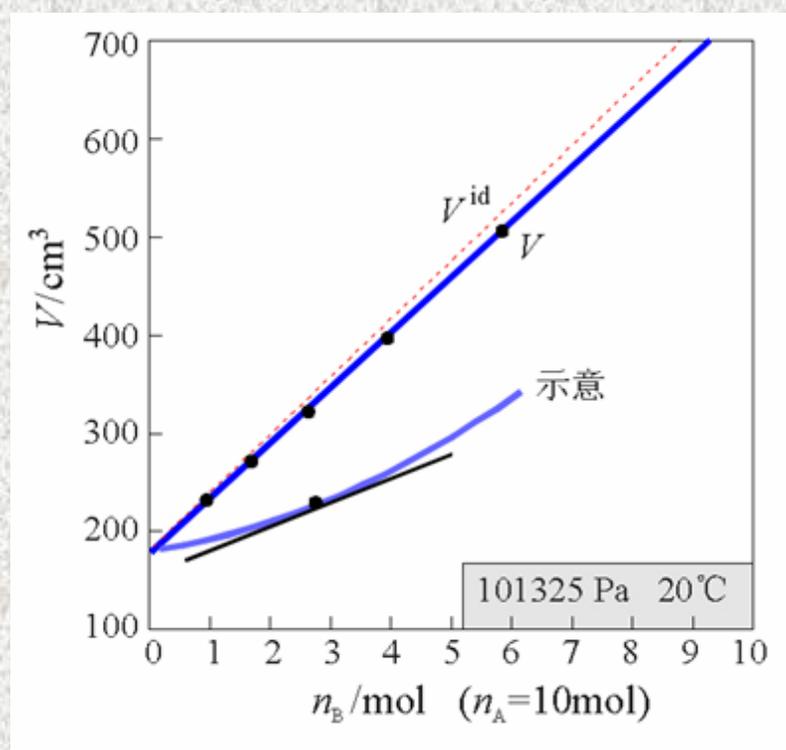
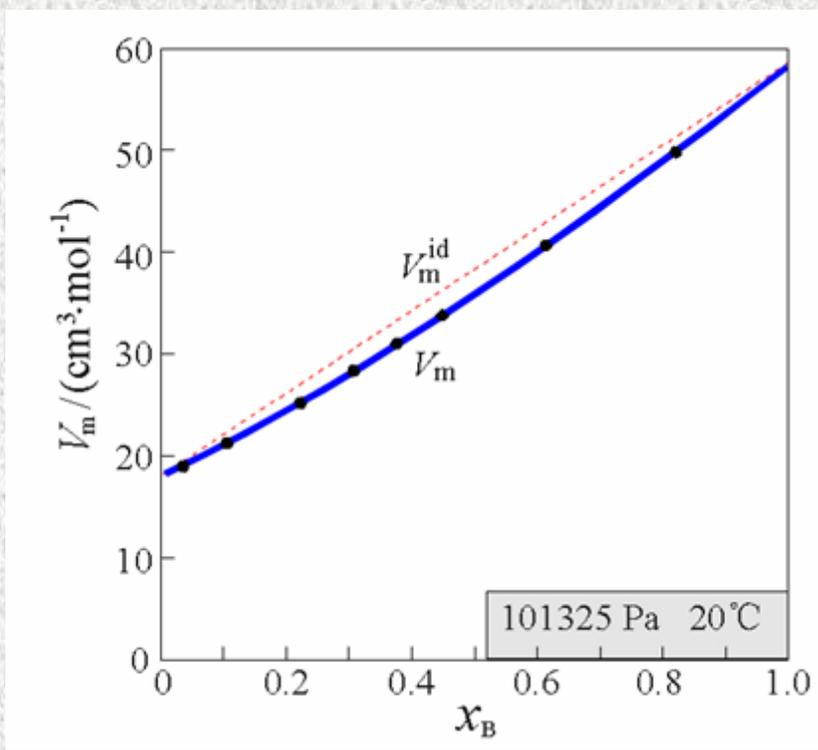
$$V_m^{\text{id}} = x_A V_A^* + x_B V_B^*$$

表 3-1 101325Pa, 20°C C<sub>2</sub>H<sub>5</sub>OH(B) 与 H<sub>2</sub>O(A) 混合时的体积变化

$x_B$	$\frac{V_m^{\text{id}}}{\text{cm}^3 \cdot \text{mol}^{-1}}$	$\frac{V_m}{\text{cm}^3 \cdot \text{mol}^{-1}}$	$\frac{\Delta V_m}{\text{cm}^3 \cdot \text{mol}^{-1}}$	$n_B / \text{mol}$ ( $n_A = 10\text{mol}$ )	$V^{\text{id}} / \text{cm}^3$ ( $n_A = 10\text{mol}$ )	$V / \text{cm}^3$ ( $n_A = 10\text{mol}$ )
0.0416	19.76	19.54	-0.22	0.4345	206.23	203.85
0.0891	21.67	21.18	-0.49	0.9776	237.93	232.48
0.1435	23.87	23.11	-0.76	1.6759	278.69	269.81
0.2068	26.42	25.47	-0.95	2.6070	333.04	321.06
0.2811	29.41	28.34	-1.07	3.9105	409.12	394.27
0.3697	32.98	31.86	-1.12	5.8657	523.24	505.41
0.4771	37.31	36.19	-1.12	9.1247	713.47	692.07
0.6100	42.66	41.65	-1.01			
0.7787	49.46	48.73	-0.73			

# 偏摩尔量与摩尔量的区别

$$V_m^{\text{id}} = x_A V_A^* + x_B V_B^*$$



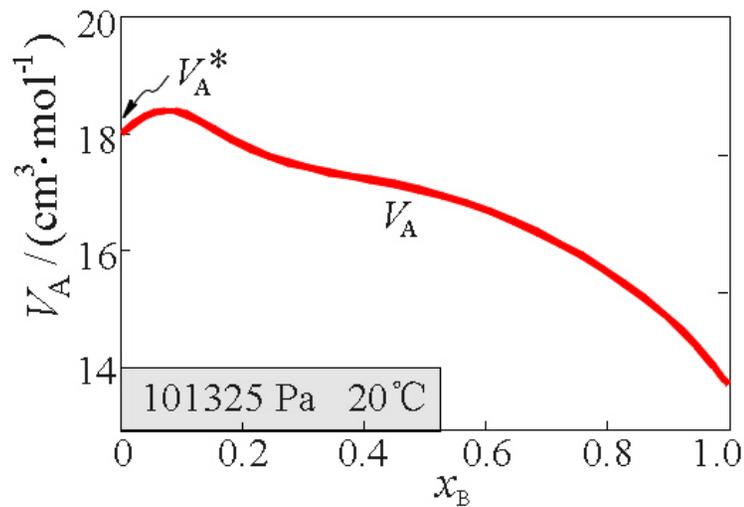
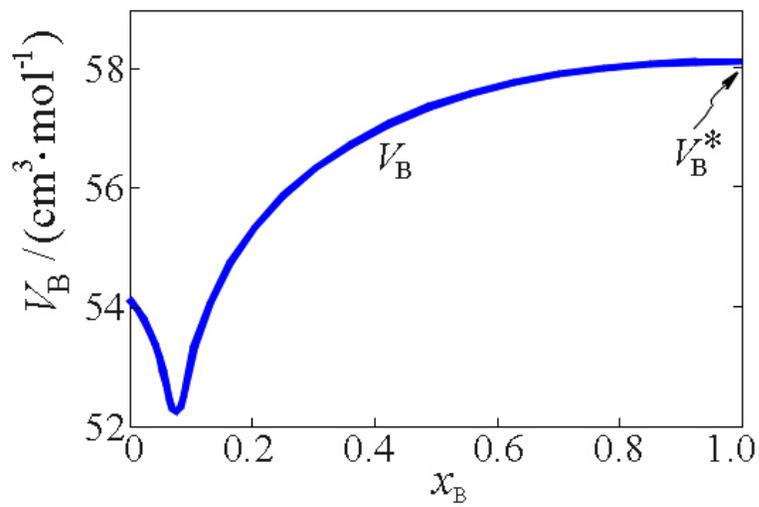
$$X_i \stackrel{\text{def}}{=} \left( \frac{\partial X}{\partial n_i} \right)_{T, p, n_{j \neq i}}$$

$X_i$  是状态函数，强度性质

$$X_i = X_i(T, p, x_1, x_2, \dots, x_{K-1})$$

$X_i$  是在系统恒定  $T$ ,  $p$  和其它物质的量时，改变 1 mol  $i$  物质引起的系统广延性质  $X$  的变化。

对纯组分系统  $X_i$  即  $X_i^*$



## 其它偏摩尔性质

$$U_i = \left( \frac{\partial U}{\partial n_i} \right)_{T, p, n_{j \neq i}}$$

$$H_i = \left( \frac{\partial H}{\partial n_i} \right)_{T, p, n_{j \neq i}}$$

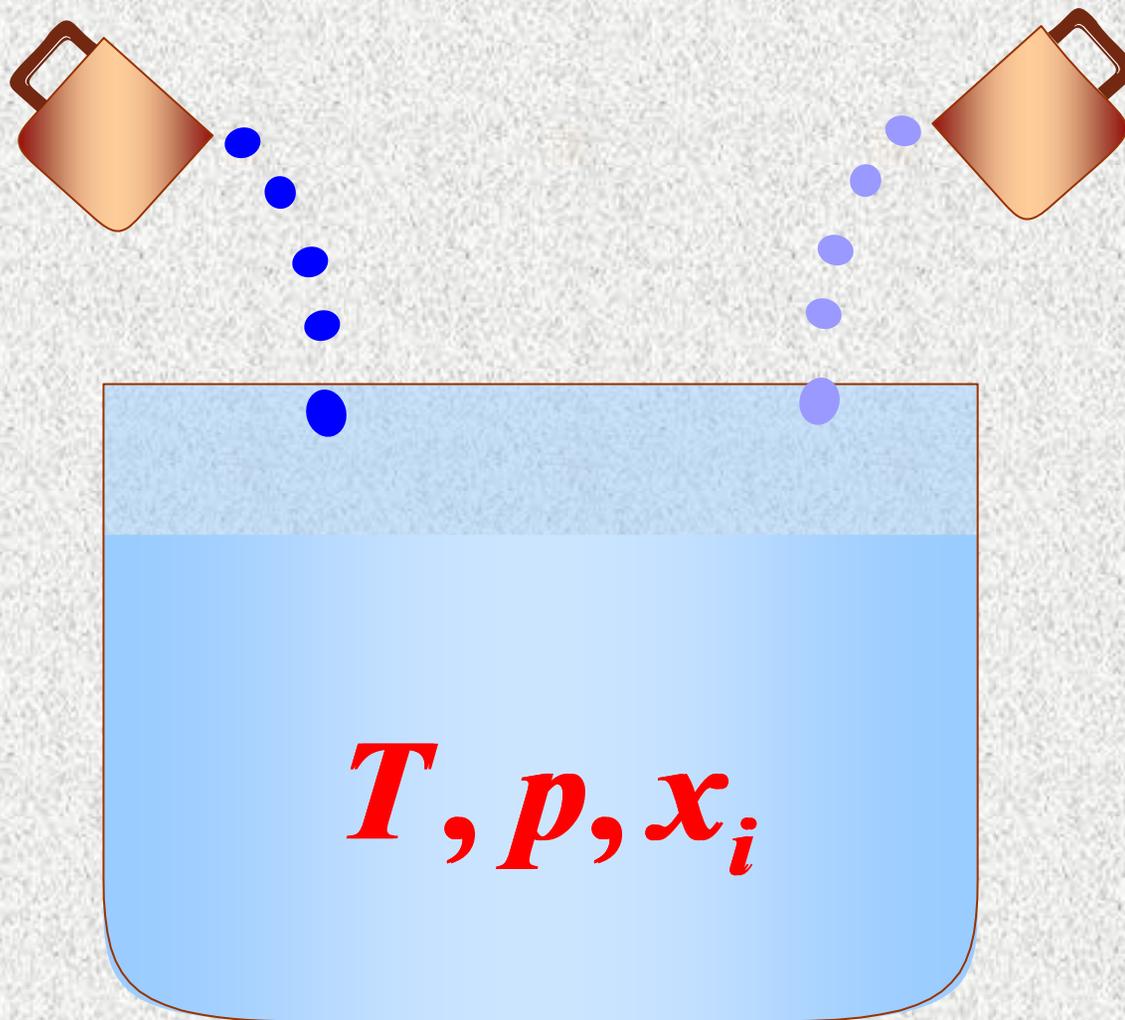
$$S_i = \left( \frac{\partial S}{\partial n_i} \right)_{T, p, n_{j \neq i}}$$

$$A_i = \left( \frac{\partial A}{\partial n_i} \right)_{T, p, n_{j \neq i}}$$

$$G_i = \left( \frac{\partial G}{\partial n_i} \right)_{T, p, n_{j \neq i}}$$

.....

## 2.集合公式



## 2. 集合公式

$$\begin{aligned}V &= \int_0^V dV = \int_0^{n_1} V_1 dn_1 + \int_0^{n_2} V_2 dn_2 \\ &= n_1 V_1 + n_2 V_2\end{aligned}$$

$$\begin{aligned}X &= \int_0^X dX = \int_0^{n_1} X_1 dn_1 + \int_0^{n_2} X_2 dn_2 + \cdots \\ &= n_1 X_1 + n_2 X_2 + \cdots \\ &= \sum_{i=1}^K n_i X_i\end{aligned}$$

### 3. 吉布斯-杜亥姆方程

$$X = \sum_{i=1}^K n_i X_i \quad dX = \sum_{i=1}^K (n_i dX_i + X_i dn_i)$$

$$dX = \left( \frac{\partial X}{\partial T} \right)_{p, n_j} dT + \left( \frac{\partial X}{\partial p} \right)_{T, n_j} dp + \sum_{i=1}^K X_i dn_i$$

$$\sum_{i=1}^K n_i dX_i = \left( \frac{\partial X}{\partial T} \right)_{p, n_j} dT + \left( \frac{\partial X}{\partial p} \right)_{T, n_j} dp$$

恒温恒压:  $\sum_{i=1}^K n_i dX_i = 0 \quad \sum_{i=1}^K x_i dX_i = 0$

二元系统:  $x_A dX_A + x_B dX_B = 0$

## 4.同一组分的各种偏摩尔量之间的关系

$$X \longrightarrow X_i$$

$$dU = TdS - pdV$$

$$dH = TdS + Vdp$$

$$dA = -SdT - pdV$$

$$dG = -SdT + Vdp$$



$$dU_i = TdS_i - p dV_i$$

$$dH_i = TdS_i + V_i dp$$

$$dA_i = -S_i dT - p dV_i$$

$$dG_i = -S_i dT + V_i dp$$

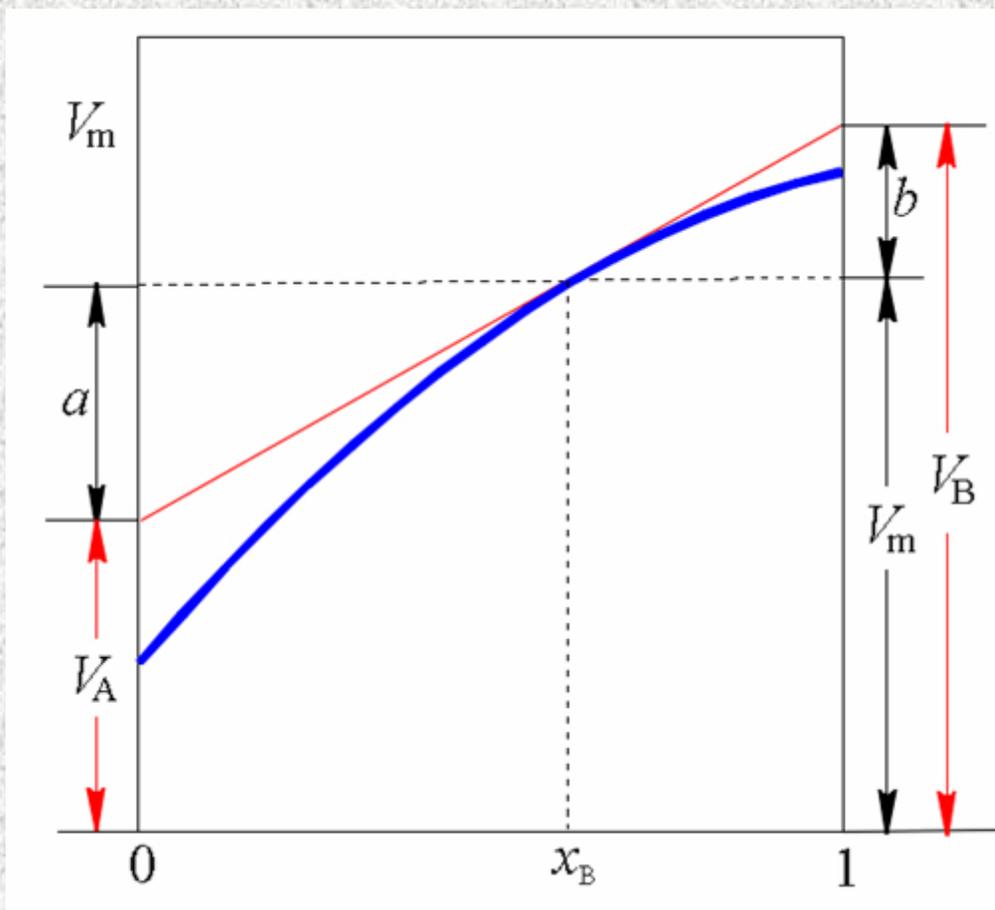
## 5. 偏摩尔量的实验测定

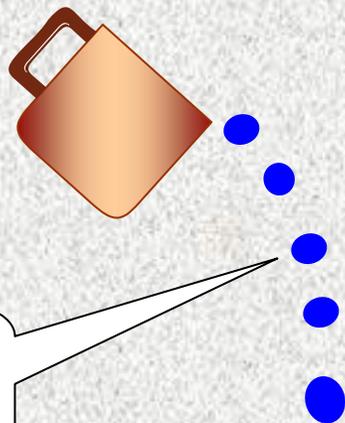
◆ 解析法

◆ 图解法

切线法

截距法

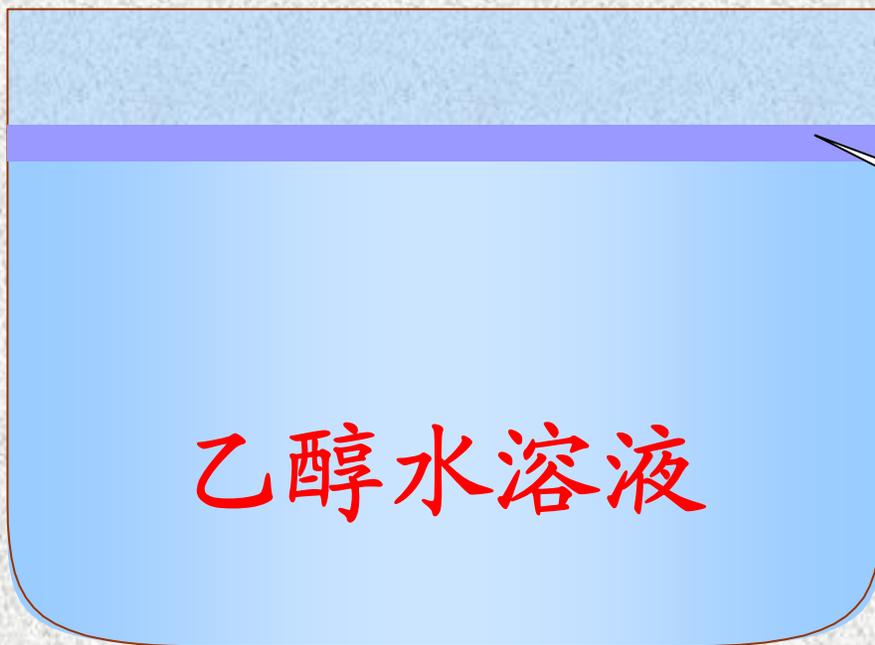




1mol乙醇  
体积 $V^*$

$$V_{\text{乙醇}} = \frac{\Delta V_{\text{溶液}}}{n_{\text{乙醇}}}$$

$$V_{\text{乙醇}} \neq V_{\text{乙醇}}^*$$



$\Delta V_{\text{溶液}}$

乙醇水溶液

# 3-3 化学势与多组分系 统的热力学基本方程

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# 1. 组成可变的均相多组分系统

$$G = G(T, p, n_1, n_2, \dots, n_K)$$

$$dG = \left( \frac{\partial G}{\partial T} \right)_{p, n_j} dT + \left( \frac{\partial G}{\partial p} \right)_{T, n_j} dp + \sum_{i=1}^K \left( \frac{\partial G}{\partial n_i} \right)_{T, p, n_{j \neq i}} dn_i$$

$$= \left( \frac{\partial G}{\partial T} \right)_{p, n_j} dT + \left( \frac{\partial G}{\partial p} \right)_{T, n_j} dp + \sum_{i=1}^K G_i dn_i$$

$$\mu_i \stackrel{\text{def}}{=} G_i = \left( \frac{\partial G}{\partial n_i} \right)_{T, p, n_{j \neq i}}$$

$$dG = \left( \frac{\partial G}{\partial T} \right)_{p, n_j} dT + \left( \frac{\partial G}{\partial p} \right)_{T, n_j} dp + \sum_{i=1}^K \mu_i dn_i$$

$$dn_i = 0 \quad \longrightarrow \quad dG = \left( \frac{\partial G}{\partial T} \right)_{p, n_j} dT + \left( \frac{\partial G}{\partial p} \right)_{T, n_j} dp$$

$$\text{组成不变} \quad \longrightarrow \quad dG = -SdT + Vdp$$

$$\left( \frac{\partial G}{\partial T} \right)_{p, n_j} = -S \qquad \left( \frac{\partial G}{\partial p} \right)_{T, n_j} = V$$

## 组成可变的均相多组分系统热力学基本方程

$$dG = -SdT + Vdp + \sum_{i=1}^K \mu_i dn_i$$

$$dA = -SdT - pdV + \sum_{i=1}^K \mu_i dn_i$$

$$dH = TdS + Vdp + \sum_{i=1}^K \mu_i dn_i$$

$$dU = TdS - pdV + \sum_{i=1}^K \mu_i dn_i$$

$$0 = SdT - Vdp + \sum_{i=1}^K n_i d\mu_i$$

适用均相封闭系统和均相敞开系统只做体积功的任意过程

$$G = G(T, p, n_1, n_2, \dots, n_K)$$

$$dG = \left( \frac{\partial G}{\partial T} \right)_{p, n_j} dT + \left( \frac{\partial G}{\partial p} \right)_{T, n_j} dp + \sum_{i=1}^K \left( \frac{\partial G}{\partial n_i} \right)_{T, p, n_{j \neq i}} dn_i$$

$$dA = \left( \frac{\partial A}{\partial T} \right)_{V, n_j} dT + \left( \frac{\partial A}{\partial V} \right)_{T, n_j} dV + \sum_{i=1}^K \left( \frac{\partial A}{\partial n_i} \right)_{T, V, n_{j \neq i}} dn_i$$

$$dH = \left( \frac{\partial H}{\partial S} \right)_{p, n_j} dS + \left( \frac{\partial H}{\partial p} \right)_{S, n_j} dp + \sum_{i=1}^K \left( \frac{\partial H}{\partial n_i} \right)_{S, p, n_{j \neq i}} dn_i$$

$$dU = \left( \frac{\partial U}{\partial S} \right)_{V, n_j} dS + \left( \frac{\partial U}{\partial V} \right)_{S, n_j} dV + \sum_{i=1}^K \left( \frac{\partial U}{\partial n_i} \right)_{S, V, n_{j \neq i}} dn_i$$

$$dG = -SdT + Vdp + \sum_{i=1}^K \mu_i dn_i$$

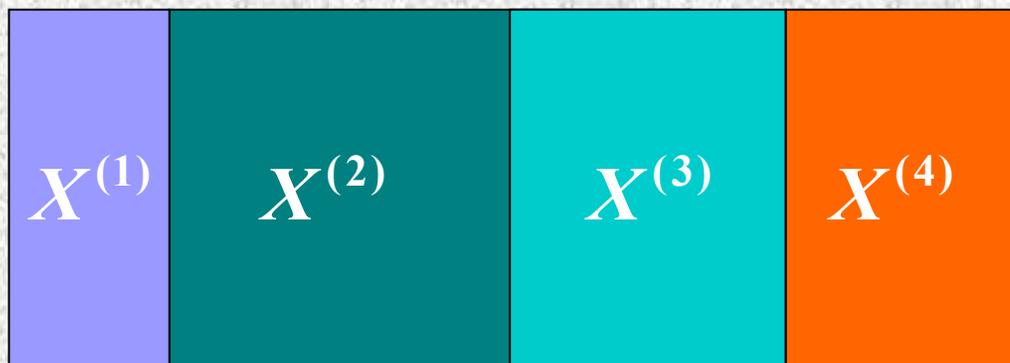
$$dA = -SdT - pdV + \sum_{i=1}^K \mu_i dn_i$$

$$dH = TdS + Vdp + \sum_{i=1}^K \mu_i dn_i$$

$$dU = TdS - pdV + \sum_{i=1}^K \mu_i dn_i$$

$$\mu_i = \left( \frac{\partial G}{\partial n_i} \right)_{T,p,n_{j \neq i}} = \left( \frac{\partial A}{\partial n_i} \right)_{T,V,n_{j \neq i}} = \left( \frac{\partial H}{\partial n_i} \right)_{S,p,n_{j \neq i}} = \left( \frac{\partial U}{\partial n_i} \right)_{S,V,n_{j \neq i}}$$

## 2. 组成可变的相多组分系统



$$X = X^{(1)} + X^{(2)} + \cdots + X^{(\pi)} = \sum_{\alpha=1}^{\pi} X^{(\alpha)}$$

$$dX = dX^{(1)} + dX^{(2)} + \cdots + dX^{(\pi)} = \sum_{\alpha=1}^{\pi} dX^{(\alpha)}$$

## 2. 组成可变的相多组分系统

$$dU^{(1)} = TdS^{(1)} - pdV^{(1)} + \sum_{i=1}^K \mu_i^{(1)} dn_i^{(1)}$$

+

$$dU^{(2)} = TdS^{(2)} - pdV^{(2)} + \sum_{i=1}^K \mu_i^{(2)} dn_i^{(2)}$$

||

$$dU = TdS - pdV + \sum_{\alpha=1}^{\pi} \sum_{i=1}^K \mu_i^{(\alpha)} dn_i^{(\alpha)}$$

## 组成可变的相多组分系统的热力学基本方程

$$dU = TdS - pdV + \sum_{\alpha=1}^{\pi} \sum_{i=1}^K \mu_i^{(\alpha)} dn_i^{(\alpha)}$$

$$dH = TdS - Vdp + \sum_{\alpha=1}^{\pi} \sum_{i=1}^K \mu_i^{(\alpha)} dn_i^{(\alpha)}$$

$$dA = -SdT - pdV + \sum_{\alpha=1}^{\pi} \sum_{i=1}^K \mu_i^{(\alpha)} dn_i^{(\alpha)}$$

$$dG = -SdT + Vdp + \sum_{\alpha=1}^{\pi} \sum_{i=1}^K \mu_i^{(\alpha)} dn_i^{(\alpha)}$$

$$0 = SdT - Vdp + \sum_{\alpha=1}^{\pi} \sum_{i=1}^K n_i^{(\alpha)} d\mu_i^{(\alpha)}$$

适用封闭系统和敞开系统只做体积功的任意过程

### 3. 绝对活度

$$\lambda_i \stackrel{\text{def}}{=} \exp \frac{\mu_i}{RT}$$

$$\mu_i = RT \ln \lambda_i$$

# 3-4 平衡判据 与平衡条件

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$$dS_{U,V,W'=0} \geq 0 \quad dA_{T,V,W'=0} \leq 0 \quad dG_{T,p,W'=0} \leq 0$$



$$T_{\text{环}} dS - dQ \geq 0$$



**热力学第二定律**

$$T_{\text{环}}dS - dQ \geq 0$$

$$dU = dQ + dW$$


$$dU \leq TdS - pdV$$

$$dH \leq TdS + Vdp$$

$$dA \leq -SdT - pdV$$

$$dG \leq -SdT + Vdp$$

$$dU \leq TdS - pdV$$

$$dH \leq TdS + Vdp$$

$$dA \leq -SdT - pdV$$

$$dG \leq -SdT + Vdp$$

$$dU = TdS - pdV + \sum_{\alpha=1}^{\pi} \sum_{i=1}^K \mu_i^{(\alpha)} dn_i^{(\alpha)}$$

$$dH = TdS + Vdp + \sum_{\alpha=1}^{\pi} \sum_{i=1}^K \mu_i^{(\alpha)} dn_i^{(\alpha)}$$

$$dA = -SdT - pdV + \sum_{\alpha=1}^{\pi} \sum_{i=1}^K \mu_i^{(\alpha)} dn_i^{(\alpha)}$$

$$dG = -SdT + Vdp + \sum_{\alpha=1}^{\pi} \sum_{i=1}^K \mu_i^{(\alpha)} dn_i^{(\alpha)}$$

$$\sum_{\alpha=1}^{\pi} \sum_{i=1}^K \mu_i^{(\alpha)} dn_i^{(\alpha)} \leq 0$$

适用于封闭系统只做体积功时相变化和化学变化的平衡判据

# 1. 平衡判据

$$\sum_{\alpha=1}^{\pi} \sum_{i=1}^K \mu_i^{(\alpha)} \mathrm{d}n_i^{(\alpha)} \leq 0$$

适用于封闭系统  
只做体积功时相  
变化和化学变化  
的平衡判据

$$\mathrm{d}U_{S,V} =$$

$$\mathrm{d}H_{S,p} =$$

$$\mathrm{d}A_{T,V} =$$

$$\mathrm{d}G_{T,p} =$$

$$\sum_{\alpha=1}^{\pi} \sum_{i=1}^K \mu_i^{(\alpha)} \mathrm{d}n_i^{(\alpha)} \leq 0$$

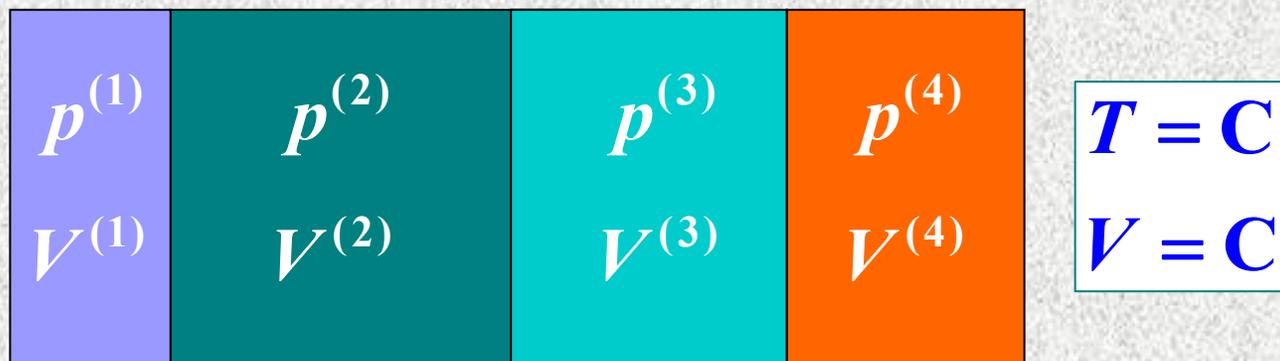
## 2. 热平衡条件

按热力学第零定律，当系统处于热平衡时，各相的温度必定相等

$$T^{(1)} = T^{(2)} = \dots = T^{(\pi)} = T$$

当两个系统各自与第三个系统达到热平衡时，这两个系统彼此也达到热平衡

### 3. 力平衡条件

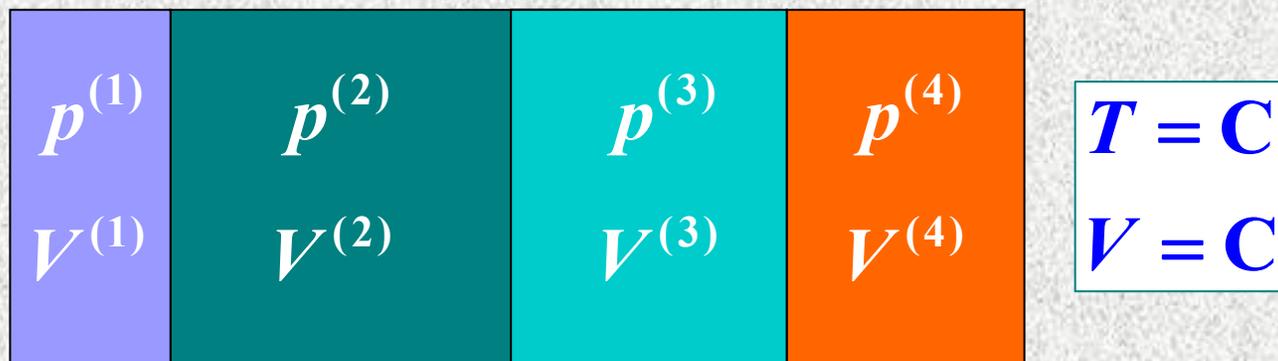


$$dT = 0, \quad dV = 0, \quad \sum_{\alpha=1}^{\pi} \sum_{i=1}^K \mu_i^{(\alpha)} dn_i^{(\alpha)} = 0$$

$$dA_{T,V} = -p^{(1)}dV^{(1)} - p^{(2)}dV^{(2)} - \dots - p^{(\pi)}dV^{(\pi)}$$

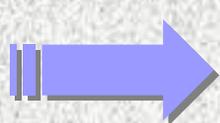
$$dV = dV^{(1)} + dV^{(2)} + \dots + dV^{(\pi)} = 0$$

### 3. 力平衡条件



$$dA_{T,V} = -p^{(1)}(-dV^{(2)} - dV^{(3)} \dots) - p^{(2)}dV^{(2)} \dots = 0$$

$$dA_{T,V} = (p^{(1)} - p^{(2)})dV^{(2)} + \dots + (p^{(1)} - p^{(\pi)})dV^{(\pi)} = 0$$



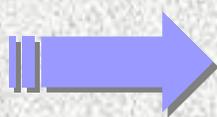
$$p^{(1)} = p^{(2)} = \dots = p^{(\pi)} = p$$

## 4. 相平衡条件

$$\sum_{\alpha=1}^{\pi} \sum_{i=1}^K \mu_i^{(\alpha)} \mathrm{d}n_i^{(\alpha)} = 0$$

$$\mathrm{d}n_i = \mathrm{d}n_i^{(1)} + \mathrm{d}n_i^{(2)} + \cdots + \mathrm{d}n_i^{(\pi)} = 0$$

$$\sum_{i=1}^K [(\mu_i^{(2)} - \mu_i^{(1)}) \mathrm{d}n_i^{(2)} + \cdots + (\mu_i^{(\pi)} - \mu_i^{(1)}) \mathrm{d}n_i^{(\pi)}] = 0$$



$$\mu_i^{(1)} = \mu_i^{(2)} = \cdots = \mu_i^{(\pi)}$$

$$\mu_i^{(1)} > \mu_i^{(2)}$$

## 5. 化学平衡条件

$$0 = \sum_{\text{B}} \nu_{\text{B}} \mathbf{B} = -e\text{E} - f\text{F} - \dots + g\text{G} + r\text{R} + \dots$$

$$\sum_{\alpha=1}^{\pi} \sum_{i=1}^K \mu_i^{(\alpha)} \mathbf{d}n_i^{(\alpha)}$$

$$= \mu_{\text{E}} \mathbf{d}n_{\text{E}} + \mu_{\text{F}} \mathbf{d}n_{\text{F}} + \mu_{\text{G}} \mathbf{d}n_{\text{G}} + \mu_{\text{R}} \mathbf{d}n_{\text{R}} + \dots$$

$$= (-e\mu_{\text{E}} - f\mu_{\text{F}} + g\mu_{\text{G}} + r\mu_{\text{R}} + \dots) \mathbf{d}\xi$$

$$= \sum_{\text{B}} \nu_{\text{B}} \mu_{\text{B}} \mathbf{d}\xi = 0$$

$$\mathbf{d}\xi \neq 0$$



$$\sum_{\text{B}} \nu_{\text{B}} \mu_{\text{B}} = 0$$

$$0 = \sum_{\text{B}} \nu_{\text{B}} \mathbf{B} = -e\mathbf{E} - f\mathbf{F} - \dots + g\mathbf{G} + r\mathbf{R} + \dots$$

$$\sum_{\alpha=1}^{\pi} \sum_{i=1}^K \mu_i^{(\alpha)} \mathrm{d}n_i^{(\alpha)}$$

$$= (-e\mu_{\text{E}} - f\mu_{\text{F}} + g\mu_{\text{G}} + r\mu_{\text{R}} + \dots) \mathrm{d}\xi$$

$$= \sum_{\text{B}} \nu_{\text{B}} \mu_{\text{B}} \mathrm{d}\xi < 0$$

$$\sum_{\text{B}} \nu_{\text{B}} \mu_{\text{B}} < 0$$

$$\mathrm{d}\xi > 0$$

$$\sum_{\text{B}} \nu_{\text{B}} \mu_{\text{B}} > 0$$

$$\mathrm{d}\xi < 0$$

## 系统平衡条件

热平衡  $T^{(1)} = T^{(2)} = \dots = T^{(\pi)}$

力平衡  $p^{(1)} = p^{(2)} = \dots = p^{(\pi)}$

相平衡  $\mu_i^{(1)} = \mu_i^{(2)} = \dots = \mu_i^{(\pi)}$

化学平衡  $\sum_{\text{B}} \nu_{\text{B}} \mu_{\text{B}} = 0$

## 各类平衡判据（可逆性判据）应用条件

$$T_{\text{环}} dS - dQ \geq 0$$

$$\sum_{\alpha=1}^{\pi} \sum_{i=1}^K \mu_i^{(\alpha)} dn_i^{(\alpha)} \leq 0$$

$$dS_{U,V,W'=0} \geq 0$$

$$dS_Q \geq 0$$

$$dA_{T,V,W'=0} \leq 0$$

$$dG_{T,p,W'=0} \leq 0$$

$$T^{(\alpha)} = T^{(\beta)} = T$$

$$p^{(\alpha)} = p^{(\beta)} = p$$

$$\mu_i^{(\alpha)} = \mu_i^{(\beta)} = \mu_i^{(\pi)}$$

$$\sum_B \nu_B \mu_B = 0$$

## 各类平衡判据（可逆性判据）应用条件

$$T_{\text{环}} dS - dQ \geq 0$$

封闭系统，任意过程。

$$dS_{U,V,W'=0} \geq 0$$

$$dS_Q \geq 0$$

$$dA_{T,V,W'=0} \leq 0$$

$$dG_{T,p,W'=0} \leq 0$$

孤立系统；  
封闭系统绝热过程；  
封闭系统只做体积功，  
恒温恒容过程；  
恒温恒压过程。

## 各类平衡判据（可逆性判据）应用条件

$$T_{\text{环}} dS - dQ \geq 0$$

$$\sum_{\alpha=1}^{\pi} \sum_{i=1}^K \mu_i^{(\alpha)} dn_i^{(\alpha)} \leq 0$$

$$dS_{U,V,W'=0} \geq 0$$

$$dA_{T,V,W'=0} \leq 0$$

$$dG_{T,p,W'=0} \leq 0$$

封闭系统，  
只做体积功，  
只涉及相变化和  
化学变化过程。

## 各类平衡判据（可逆性判据）应用条件

$$T_{\text{环}} dS - dQ \geq 0$$

$$\sum_{\alpha=1}^{\pi} \sum_{i=1}^K \mu_i^{(\alpha)} dn_i^{(\alpha)} \leq 0$$

$$dS_{U,V,W'=0} \geq 0$$

$$dA_{T,V,W'=0} \leq 0$$

$$dG_{T,p,W'=0} \leq 0$$

$$\mu_i^{(\alpha)} = \mu_i^{(\beta)} = \mu_i^{(\pi)}$$

$$\sum_B \nu_B \mu_B = 0$$

封闭系统只做体积功，  
相变化 化学变化

## 各类平衡判据（可逆性判据）应用条件

$$T_{\text{环}} dS - dQ \geq 0$$

$$\sum_{\alpha=1}^{\pi} \sum_{i=1}^K \mu_i^{(\alpha)} dn_i^{(\alpha)} \leq 0$$

$$dS_{U,V,W'=0} \geq 0$$

$$dA_{T,V,W'=0} \leq 0$$

$$dG_{T,p,W'=0} \leq 0$$

$$T^{(\alpha)} = T^{(\beta)} = T$$

$$p^{(\alpha)} = p^{(\beta)} = p$$

$$\mu_i^{(\alpha)} = \mu_i^{(\beta)} = \mu_i^{(\pi)}$$

$$\sum_B \nu_B \mu_B = 0$$

## 系统平衡条件

热平衡  $T^{(1)} = T^{(2)} = \dots = T^{(\pi)}$

力平衡  $p^{(1)} = p^{(2)} = \dots = p^{(\pi)}$

相平衡  $\mu_i^{(1)} = \mu_i^{(2)} = \dots = \mu_i^{(\pi)}$

化学平衡  $\sum_{\text{B}} \nu_{\text{B}} \mu_{\text{B}} = 0$

# 3-5 相律

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# 1. 相律的推导

设系统—— $K$ 个组分， $\pi$ 个相

强度性质总数

$$T^{(1)}, p^{(1)}, x_1^{(1)}, x_2^{(1)} \cdots x_{K-1}^{(1)}$$

$$T^{(2)}, p^{(2)}, x_1^{(2)}, x_2^{(2)} \cdots x_{K-1}^{(2)}$$

.....

$$T^{(\pi)}, p^{(\pi)}, x_1^{(\pi)}, x_2^{(\pi)} \cdots x_{K-1}^{(\pi)}$$

$$\pi(K+1)$$

限制方程

$$T^{(1)} = T^{(2)} = \cdots = T^{(\pi)}$$

$$p^{(1)} = p^{(2)} = \cdots = p^{(\pi)}$$

$$\mu_i^{(1)} = \cdots = \mu_i^{(\pi)} \quad i=1 \sim K$$

$$\sum \nu_B \mu_B = 0 \quad R'$$

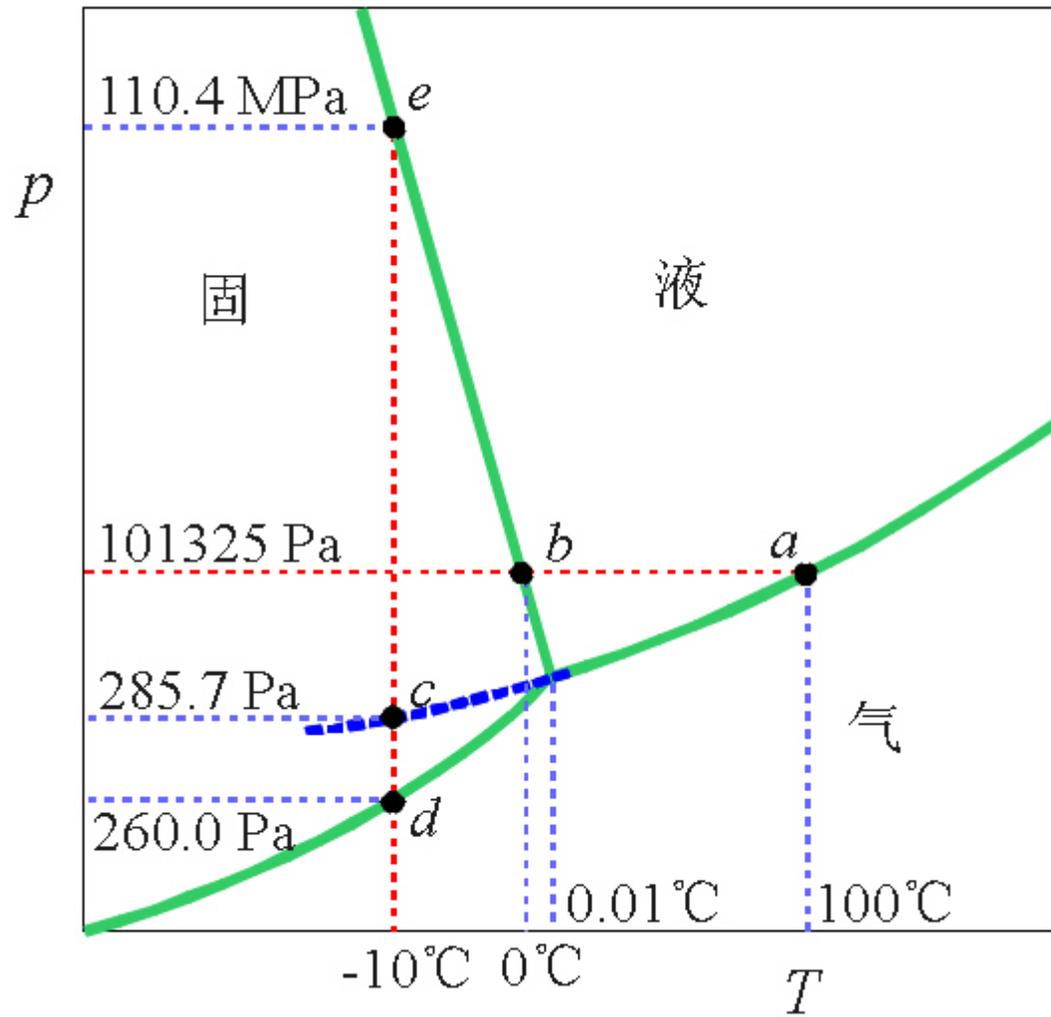
$$(\pi-1)(K+2)+R+R'$$

$$K - \pi + 2 - R - R' \quad \Rightarrow \quad f$$

$$f = K - \pi + 2 - R - R'$$

自由度  $f$ —平衡系统的强度性质中独立变量的数目

- ◆ 确定一个系统的状态所必须确定的独立强度性质的数目
- ◆ 在一定范围内可以独立变动而不致引起旧相消失或新相产生的强度性质的数目



$$f = K - \pi + 2 - R - R'$$

自由度  $f$  — 平衡系统的强度性质中独立变量的数目

- ◆ 确定一个系统的状态所必须确定的独立强度性质的数目
- ◆ 在一定范围内可以独立变动而不致引起旧相消失或新相产生的强度性质的数目

令： $K - R - R' = K'$   $\Rightarrow$  独立组分数

$$f = K' - \pi + 2$$

## 2. 相律的应用

◆ 单元系相平衡  $K = 1, R = 0, R' = 0$

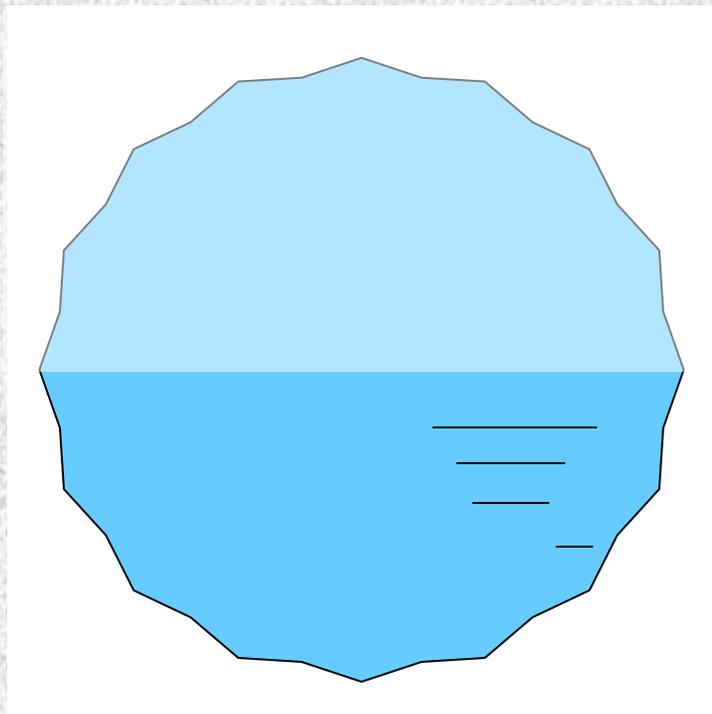
单相系统:  $\pi = 1 \quad f = 1 - 1 + 2 - 0 = 2$

两相平衡:  $\pi = 2 \quad f = 1 - 2 + 2 - 0 = 1$

三相平衡:  $\pi = 3 \quad f = 1 - 3 + 2 - 0 = 0$

◆ 多元系相平衡

◆ 多相化学平衡



水-乙醇二元VLE

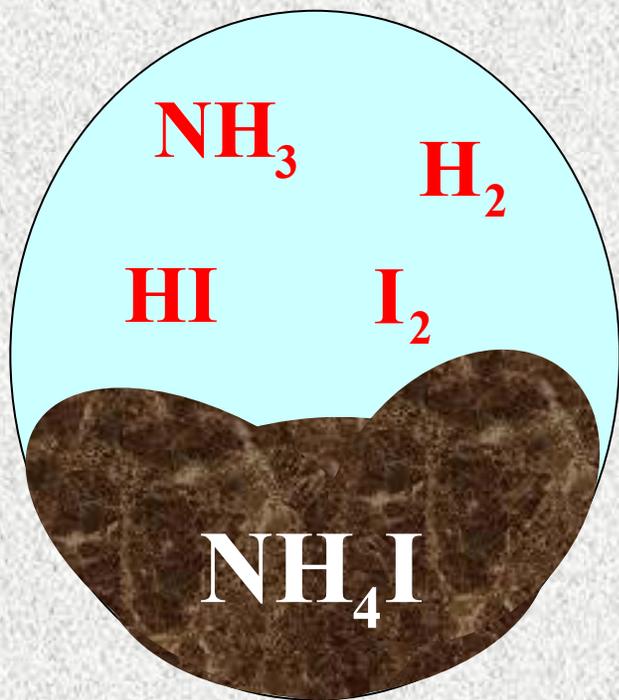
$$f = K - \pi + 2 - R - R'$$

$$f = 2 - 2 + 2 - 0 - 0 \\ = 2$$

若已知:

$$x_{\text{alc}} = 0.2, \quad f =$$

$$p = 0.1\text{MPa}, \quad f =$$



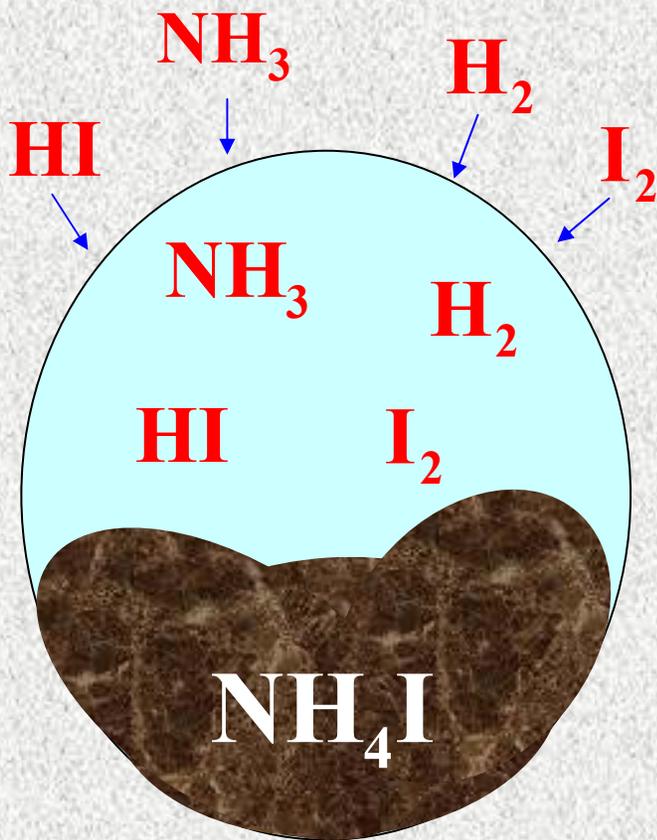
$\text{NH}_4\text{I}$ 分解达到平衡

$$f = 5 - 2 + 2 - 2 - 2 = 1$$



$$p_{\text{NH}_3} = p_{\text{HI}} + p_{\text{H}_2} + p_{\text{I}_2}$$

$$p_{\text{H}_2} = p_{\text{I}_2}$$



$$f = 5 - 2 + 2 - ? - ?$$

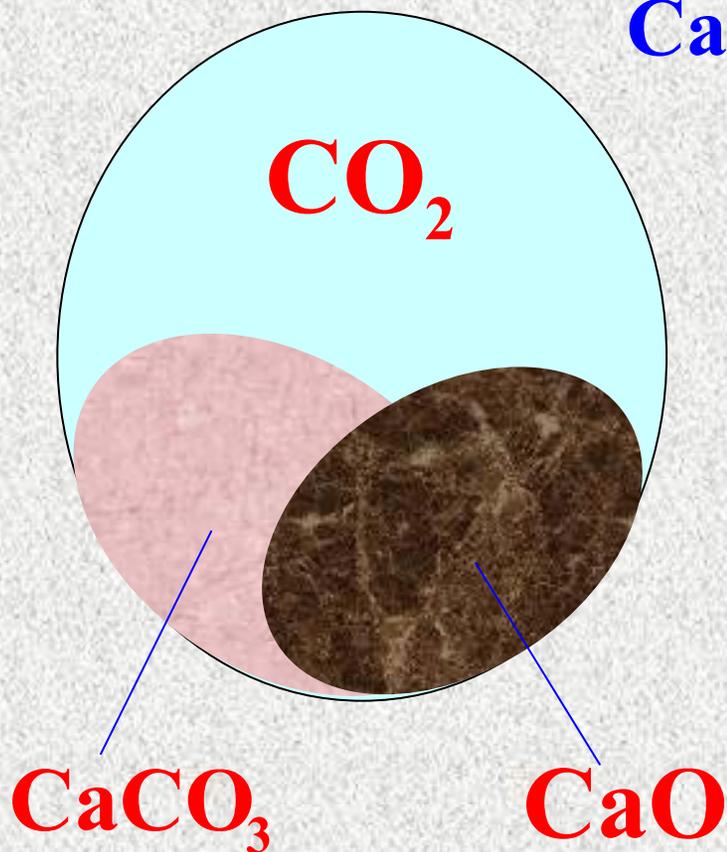
$$=$$



$$p_{\text{NH}_3} = p_{\text{HI}} + p_{\text{H}_2} + p_{\text{I}_2}$$

$$p_{\text{H}_2} = p_{\text{I}_2}$$

$\text{NH}_4\text{I}$ 分解达到平衡



$$f = 3 - 3 + 2 - 1 - 0 = 1$$

$$n_{\text{CaO}} = n_{\text{CO}_2}$$
$$R' = 1 ?$$

# 3-6 化学势与逸度

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# 1. 化学势表达式

$$\mu_i^{(\alpha)} = \mu_i^{(\beta)} \quad \Rightarrow \quad \mu_i = ?$$

$$\sum_{\text{B}} \nu_{\text{B}} \mu_{\text{B}} = 0$$

$$\mu_i = \left( \frac{\partial G}{\partial n_i} \right)_{T, p, n_{j \neq i}} \quad \mu_i = \mu_i(T, p, x_1, \dots, x_{k-1})$$

$$\left( \frac{\partial \mu_i}{\partial p} \right)_{T, x_j} = V_i \quad \left( \frac{\partial \mu_i}{\partial T} \right)_{p, x_j} = -S_i$$

$$d\mu_i = V_i dp$$

$$d\mu_i = V_i^* dp$$

## 2. 理想气体和理想气体混合物中组分的化学势表达式

### 纯理想气体

$$V_m = \frac{V}{n} = \frac{RT}{p} \quad \Rightarrow \quad d\mu_i = \left( \frac{RT}{p} \right) dp$$

$$\mu_i = \mu_i^\ominus (\text{g}) + RT \ln \frac{p}{p^\ominus}$$

$\mu_i^\ominus (\text{g})$  —  $T$  温度, 处于气体标准状态时物质的化学势  
温度为  $T$  压力为  $p^\ominus$  的理想气体  $i$  的化学势

## 理想气体混合物

$$p \quad \longrightarrow \quad p_i = py_i$$

$$\mu_i = \mu_i^\ominus (\text{g}) + RT \ln \frac{p_i}{p^\ominus}$$

$$\mu_i = \mu_i^\ominus (\text{g}) + RT \ln \frac{py_i}{p^\ominus}$$



### 3. 实际气体、液体和固体及其混合物中组分的化学势表达式

设:  $p(V_m - b) = RT \quad V_i^* = V_m = \frac{RT}{p} + b$

$$\mu_i = \mu_i^\theta(\text{g}) + RT \ln\left(\frac{p}{p^\theta}\right) + b(p - p^\theta)$$

$$b(p - p^\theta) = RT \ln \phi_i^* \quad f_i^* = p\phi_i^*$$

$$\mu_i = \mu_i^\theta(\text{g}) + RT \ln\left(\frac{p\phi_i^*}{p^\theta}\right) = \mu_i^\theta(\text{g}) + RT \ln\left(\frac{f_i^*}{p^\theta}\right)$$

## 逸度和逸度因子的定义

$$f_i(\text{或}f_i^*) \stackrel{\text{def}}{=} p^\theta \exp \frac{\mu_i - \mu_i^\theta(\text{g})}{RT}$$

$$\phi_i^* \stackrel{\text{def}}{=} f_i^* / p \quad \phi_i \stackrel{\text{def}}{=} f_i / p_i$$

纯物质

$$\begin{aligned} \mu_i &= \mu_i^\theta(\text{g}) + RT \ln(f_i^* / p^\theta) \\ &= \mu_i^\theta(\text{g}) + RT \ln(p\phi_i^* / p^\theta) \end{aligned}$$

混合物

$$\begin{aligned} \mu_i &= \mu_i^\theta(\text{g}) + RT \ln(f_i / p^\theta) \\ &= \mu_i^\theta(\text{g}) + RT \ln(p_i\phi_i / p^\theta) \end{aligned}$$

## 4. 逸度的意义

可以看作是相对于理想气体的校正压力

理想气体

$$f_i^* = p_i = p$$

理想气体混合物

$$f_i = p_i = py_i$$

实际气体、液体、固体

$$f_i^* = p_i \phi_i^* = p \phi_i^*$$

实际气液固体混合物

$$f_i = p_i \phi_i = py_i \phi_i = px_i \phi_i$$

## 4. 逸度的意义

强度性质，状态函数

$$f_i = f_i(T, p, x_1, x_2, \dots, x_{K-1})$$

压力趋于零，逸度趋于实际压力，逸度因子趋于1

$$\lim_{p \rightarrow 0} \phi_i^* = \lim_{p \rightarrow 0} (f_i^* / p) = 1 \quad \lim_{p \rightarrow 0} \phi_i = \lim_{p \rightarrow 0} (f_i / px_i) = 1$$

$\phi_i < 1$  分子间有较强的吸引倾向

$\phi_i > 1$  分子间有较强的排斥倾向

$\phi_i = 1$  吸引排斥相抵，与理想气体相当

## 4. 逸度的意义

$$\mu_i^{(\alpha)} = \mu_i^{(\beta)}$$

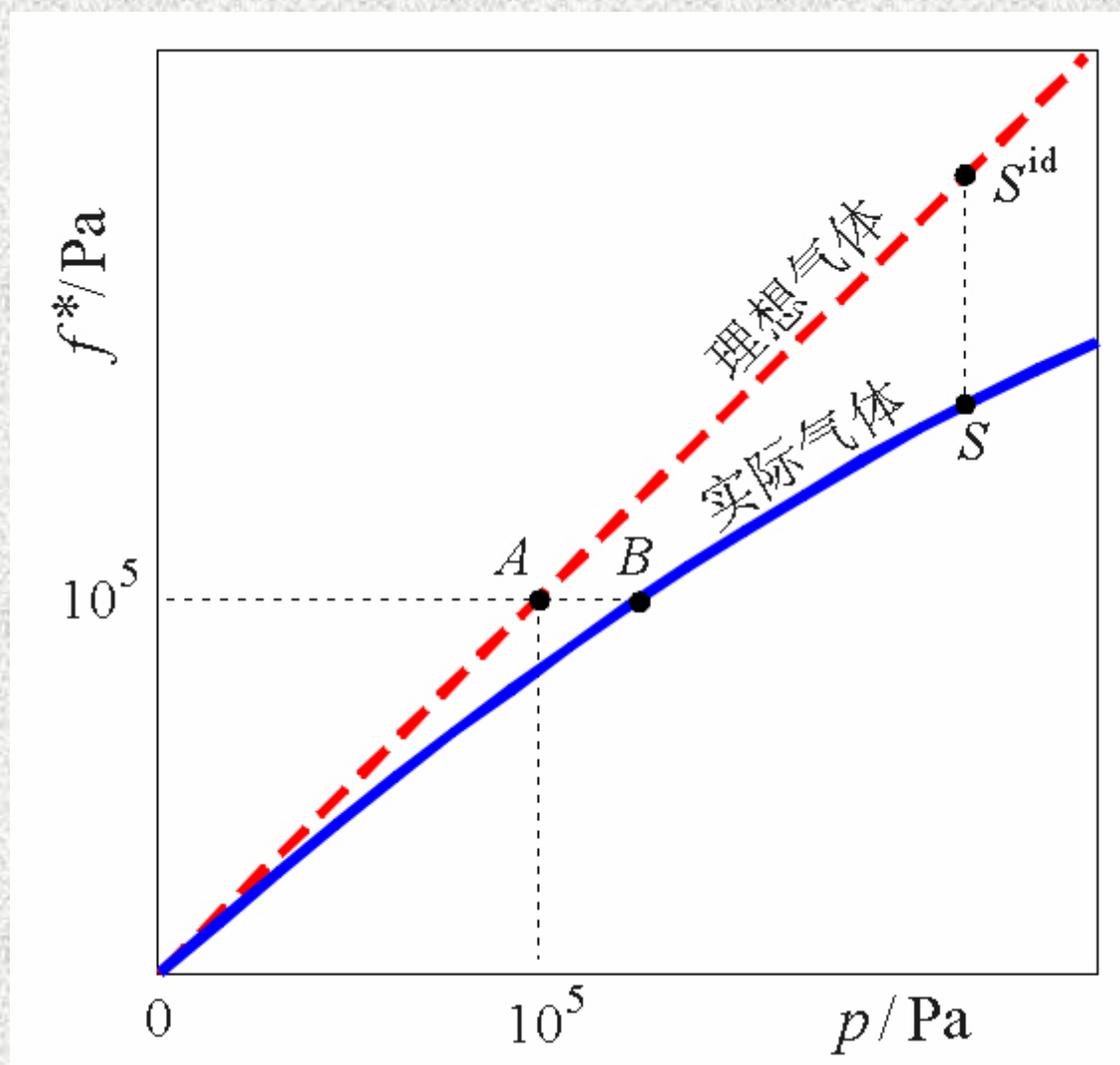


$$\mu_i^\theta(\text{g}) + RT \ln\left(\frac{f_i^{(\alpha)}}{p^\theta}\right) = \mu_i^\theta(\text{g}) + RT \ln\left(\frac{f_i^{(\beta)}}{p^\theta}\right)$$

$$f_i^{(\alpha)} = f_i^{(\beta)} = \dots = f_i^{(\pi)}$$

# 3-7 逸度和逸度 因子的求取

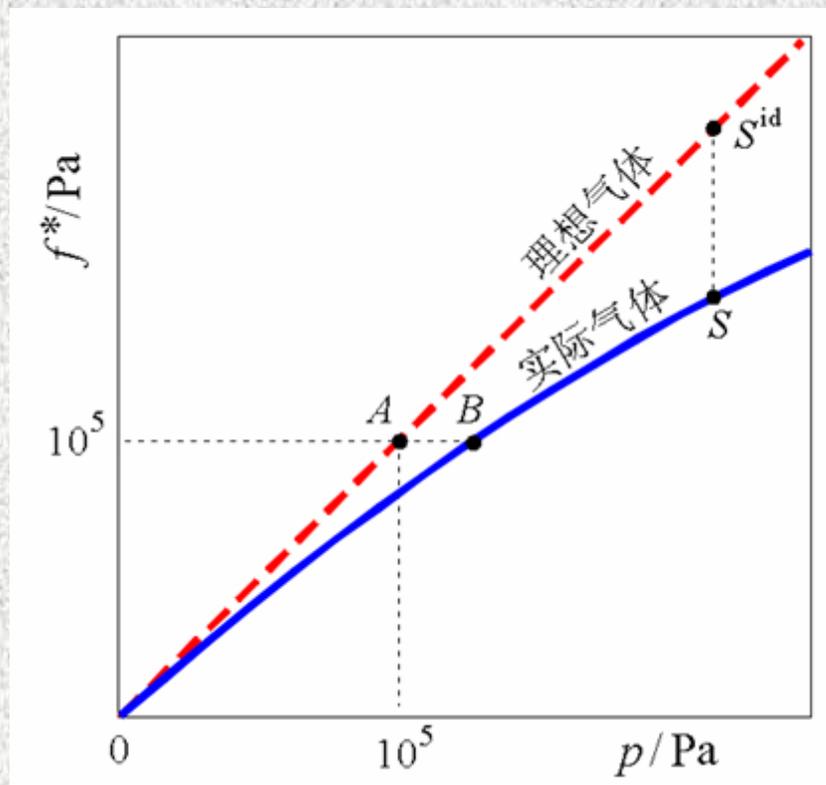
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$$\mu_i^{\text{id}} = \mu_i^\theta(\text{g}) + RT \ln \frac{p}{p^\theta}$$

$$\mu_i = \mu_i^\theta(\text{g}) + RT \ln \left( \frac{f_i^*}{p_i^\theta} \right)$$

$$\mu_i^{\text{id}} - \mu_i = RT \ln \frac{p}{f_i^*}$$



$$\mu_i^{\text{id}} - \mu_i = \int_p^0 V_i^* dp + \int_0^p V_i^{\text{id}} dp = \int_p^0 \left( V_i^* - \frac{RT}{p} \right) dp$$

$$\mu_i^{\text{id}} - \mu_i = RT \ln \frac{p}{f_i^*}$$

$$\mu_i^{\text{id}} - \mu_i = \int_p^0 V_i^* dp + \int_0^p V_i^{\text{id}} dp = \int_p^0 \left( V_i^* - \frac{RT}{p} \right) dp$$

$$\ln \phi_i^* = \ln \left( \frac{f_i^*}{p} \right) = \frac{1}{RT} \int_0^p \left( V_i^* - \frac{RT}{p} \right) dp$$

$$\ln \phi_i = \ln \left( \frac{f_i}{py_i} \right) = \frac{1}{RT} \int_0^p \left( V_i - \frac{RT}{p} \right) dp$$

$$\mu_i^{\text{id}} - \mu_i = RT \ln \frac{p}{f_i^*}$$

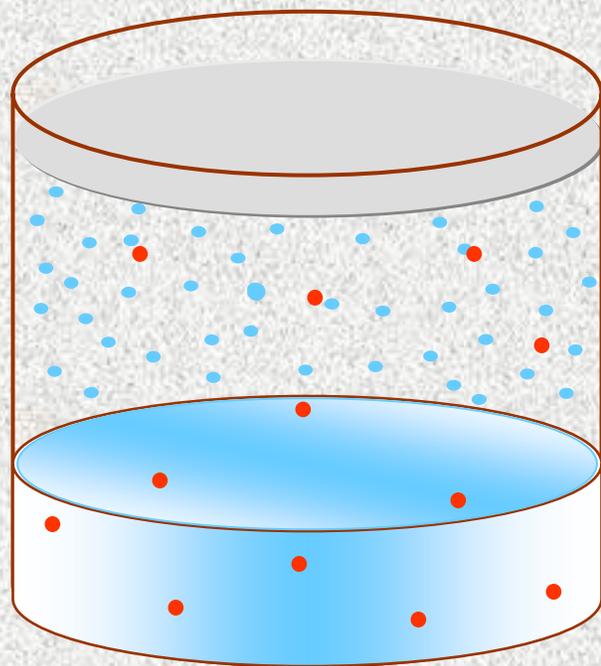
$$\mu_i^{\text{id}} - \mu_i = \int_p^0 V_i^* dp + \int_0^p V_i^{\text{id}} dp = \int_p^0 \left( V_i^* - \frac{RT}{p} \right) dp$$

$$\ln \phi_i^* = \ln \left( \frac{f_i^*}{p} \right) = \frac{1}{RT} \int_0^p \left( V_i^* - \frac{RT}{p} \right) dp$$

$$\ln \phi_i = \ln \left( \frac{f_i}{py_i} \right) = \frac{1}{RT} \int_0^p \left( V_i - \frac{RT}{p} \right) dp$$

# 3-8 稀溶液的气液平衡, 拉乌尔定律和亨利定律

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$$p = f(T, x_i, y_i)$$

# 1. 拉乌尔定律

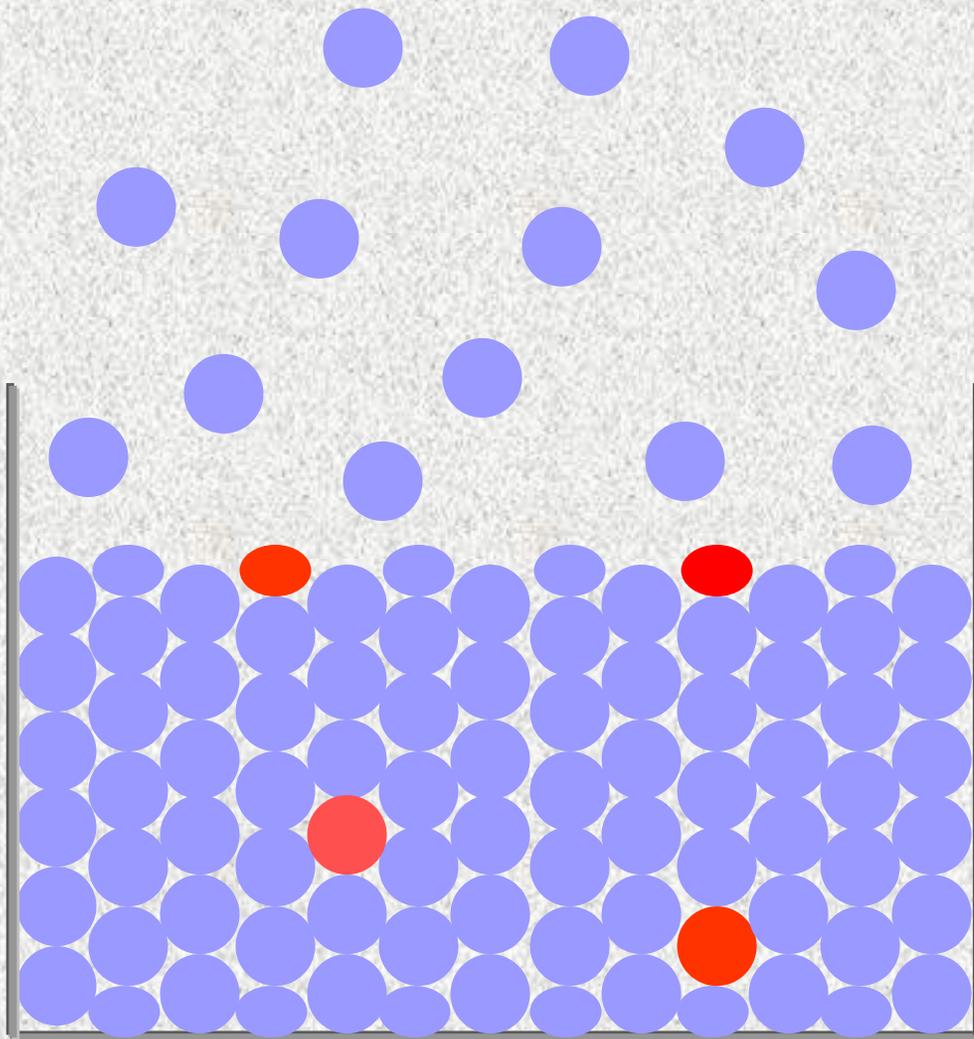
恒温下溶剂的蒸气分压等于同温度下纯溶剂的饱和蒸气压与溶液中溶剂摩尔分数的乘积，即

$$p_A = p_A^* x_A$$

## 二元系

$$x_A + x_B = 1$$

$$p_A^* - p_A = p_A^* x_B$$



# 路易斯-兰德尔规则

$$f_A = f_A^* x_A$$



$$f_i = p y_i \phi_i$$

$$f_i^* = p^* \phi_i^*$$

# 路易斯-兰德尔规则

$$f_A = f_A^* x_A$$

$$f_i = p y_i \phi_i$$

$$f_i^* = p^* \phi_i^*$$

$$\phi_i = \phi_i^*$$

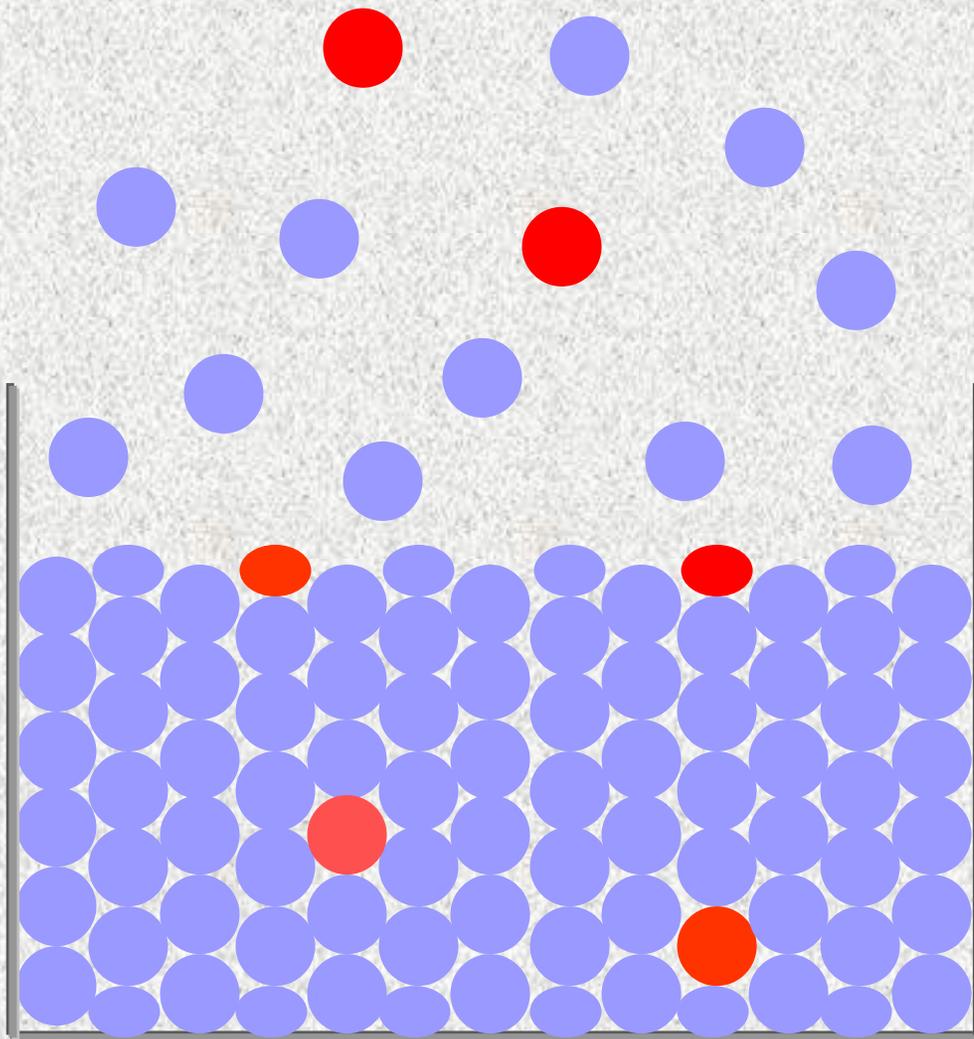
## 2. 亨利定律

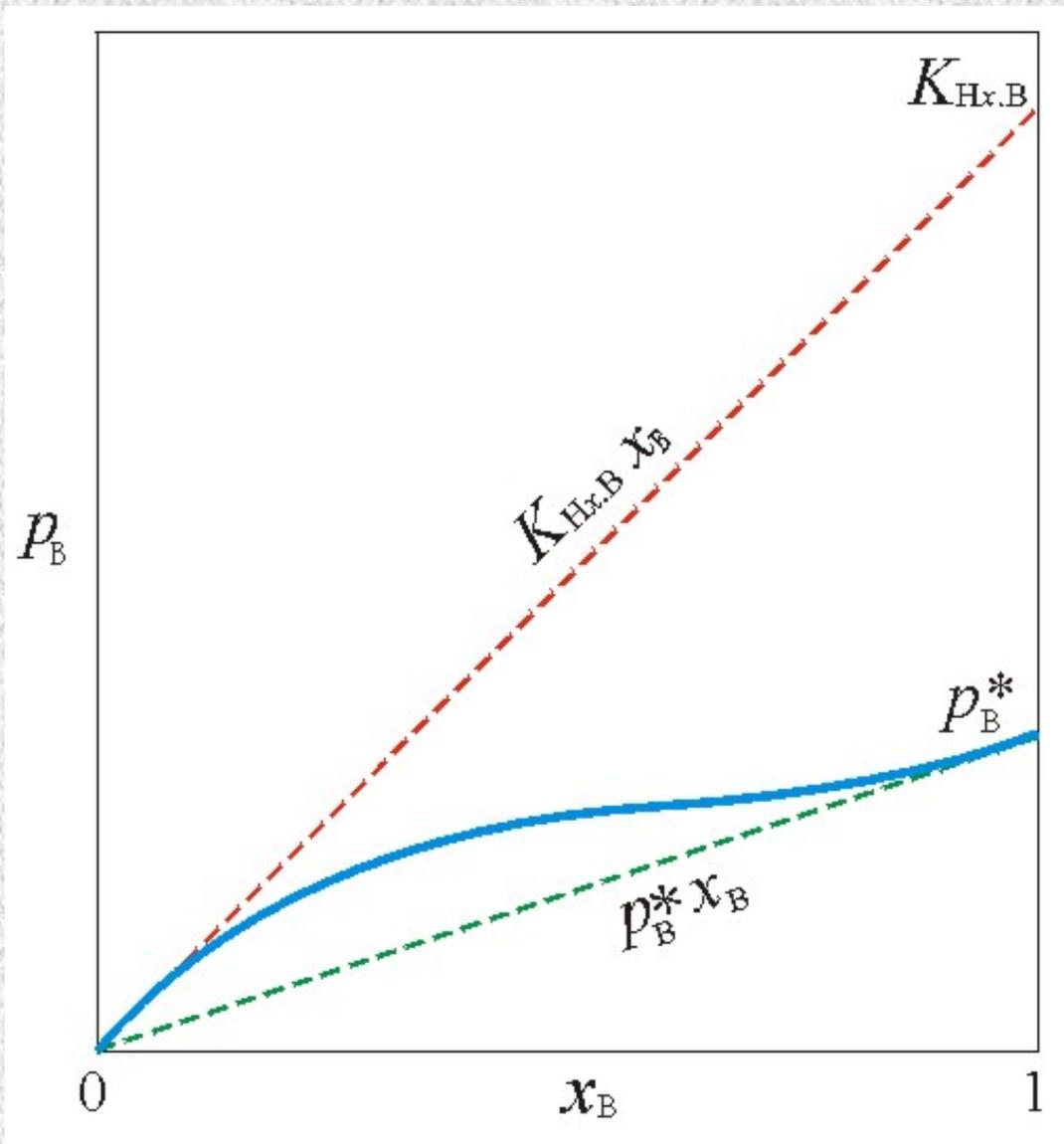
恒温下溶质的蒸气分压与溶质的摩尔分数成正比, 即

$$p_B = K_{Hx,B} x_B$$

亨利常数

$$f_B = K_{Hx,B} x_B$$





亨利常数  
 常看一拟  
 可是虚拟  
 (具有稀  
 无限液性  
 溶质的)纯  
 物质饱和  
 蒸气压

$$p_B = K_{Hx,B} x_B$$

$$p_B = K_{Hb,B} b_B$$

$$p_B = K_{Hc,B} c_B$$

# 3-9 理想混合物(理想溶液)和理想稀溶液

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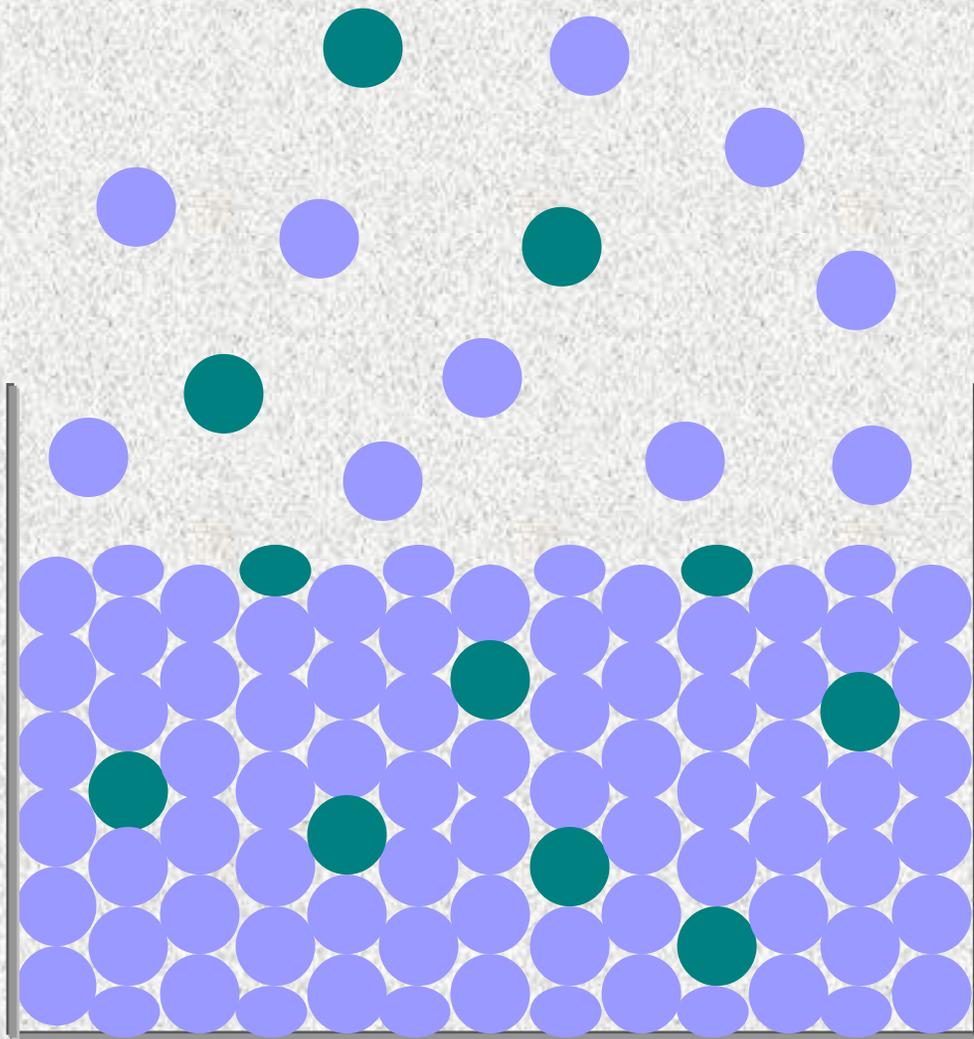
# 1. 理想混合物

所有组分在全部浓度范围内都服从拉乌尔定律的混合物。又称理想溶液

## 二元系A-B

$$p_A = p_A^* x_A \quad p_B = p_B^* x_B$$

$$p_{\text{总}} = p_A^* x_A + p_B^* x_B = p_A^* + (p_B^* - p_A^*) x_B$$



## 2. 理想稀溶液

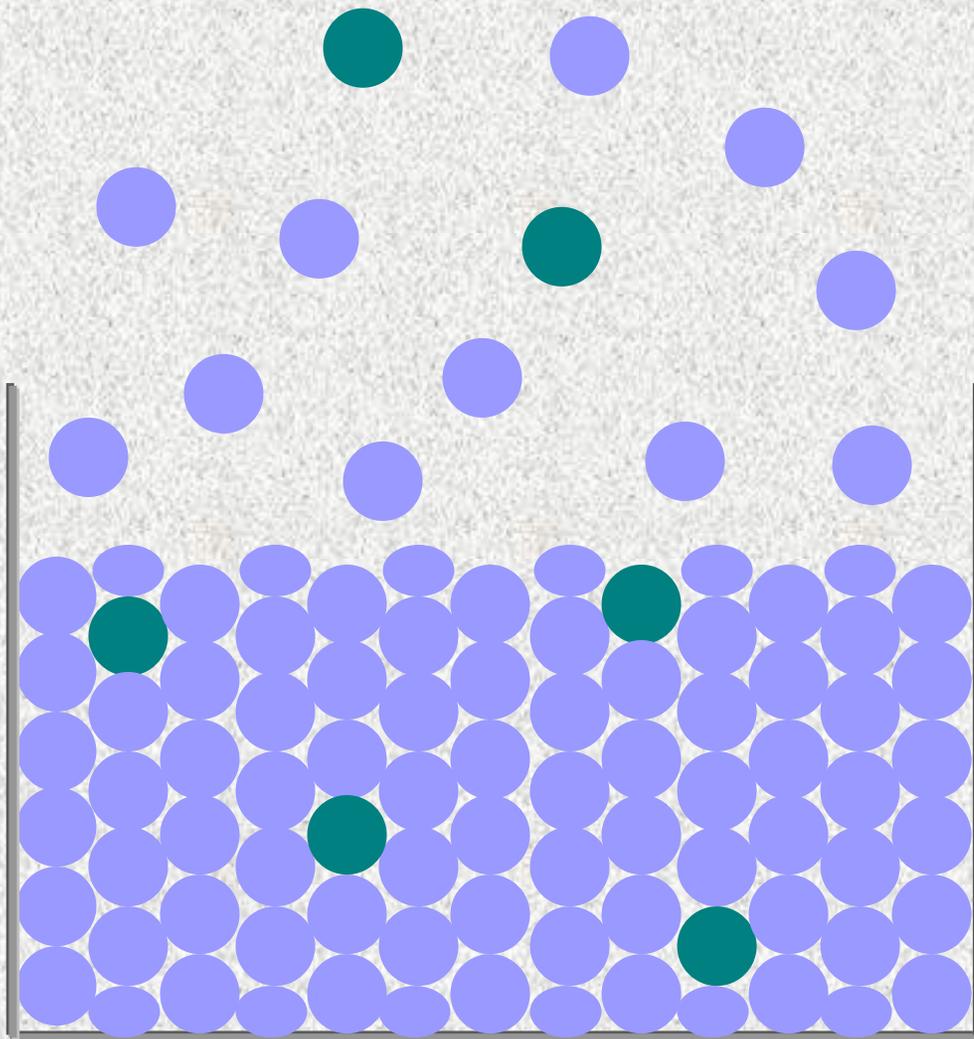
溶剂服从拉乌尔定律、溶质服从亨利定律的溶液，称为理想稀溶液

### 二元系A-B

$$p_A = p_A^* x_A$$

$$p_B = K_{Hx,B} x_B = K_{Hb,B} b_B = K_{Hc,B} c_B$$

$$\begin{aligned} p_{\text{总}} &= p_A + p_B = p_A^* x_A + K_{Hx,B} x_B \\ &= p_A^* + (K_{Hx,B} - p_A^*) x_B \end{aligned}$$



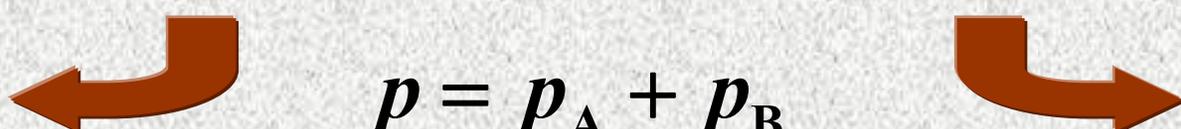
**例1** 苯(A)和甲苯(B)的混合物可看作理想混合物。20℃时它们的饱和蒸气压分别为9.96kPa和2.97kPa。试计算：(1)  $x_A=0.200$  时，混合物中苯和甲苯的分压和蒸气总压；(2) 当蒸气的  $y_A=0.200$ 时，液相的  $x_A$  和蒸气总压。

解：

拉  
乌  
尔  
定  
律

$$p_A = p_A^* x_A = p_A^* (1 - x_B) = p y_A$$

$$p_B = p_B^* x_B = p_B^* (1 - x_A) = p y_B$$


$$p = p_A + p_B$$

道  
尔  
顿  
定  
律

(1)

$$\begin{aligned} p_A &= p_A^* x_A \\ &= 9.96\text{kPa} \times 0.200 = 1.99\text{kPa} \end{aligned}$$

$$\begin{aligned} p_B &= p_B^* x_B = p_B^* (1 - x_A) \\ &= 2.97\text{kPa} \times (1 - 0.200) = 2.38\text{kPa} \end{aligned}$$

$$\begin{aligned} p &= p_A + p_B \\ &= 1.99\text{kPa} + 2.38\text{kPa} = 4.37\text{kPa} \end{aligned}$$

(2)

$$y_A = \frac{p_A}{p} = \frac{p_A^* x_A}{p_A^* x_A + p_B^* x_B}$$

$$y_A = 0.200 = \frac{9.96 x_A}{9.96 x_A + 2.97(1 - x_A)}$$

$$x_A = 0.0694$$

$$\begin{aligned} p &= p_A^* x_A + p_B^* x_B \\ &= [9.96 \times 0.0694 + 2.97 \times (1 - 0.0694)] \text{kPa} \\ &= 3.46 \text{kPa} \end{aligned}$$

# 3-10 化学势与活度

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# 相平衡条件

$$\mu_i^{\text{L}} = \mu_i^{\text{V}}$$

# 1. 理想溶液(理想混合物)

$$\begin{aligned}\mu_i^{\text{L}} &= \mu_i^{\text{V}} = \mu_i^{\ominus}(\text{g}) + RT \ln p_i / p^{\ominus} \\ &= \mu_i^{\ominus}(\text{g}) + RT \ln p_i^* / p^{\ominus} + RT \ln x_i\end{aligned}$$

惯例 I 参考  
状态  $\mu_i^*$

同温度下纯液体或纯  
固体的化学势

$$\mu_i = \mu_i^* + RT \ln x_i$$

## 2. 理想稀溶液 $p_B = K_{Hx,B} x_B$

$$\begin{aligned}\mu_B^L &= \mu_B^V = \mu_B^\ominus(\text{g}) + RT \ln p_B / p^\ominus \\ &= \mu_B^\ominus(\text{g}) + RT \ln K_{Hx,B} / p^\ominus + RT \ln x_B\end{aligned}$$

惯例 II 参考  
状态  $\mu_{x,B}^*$

同温度下虚拟纯物质  
的化学势

$$\mu_B = \mu_{x,B}^* + RT \ln x_B$$

### 3. 实际混合物及实际溶液

$$p_i = p_i^* a_i = p_i^* x_i \gamma_i \quad a \text{ —— 活度}$$

$$p_B = K_{\text{Hx},B} a_{x,B} = K_{\text{Hx},B} x_B \gamma_{x,B} \quad \gamma \text{ —— 活度因子}$$

$$\begin{aligned} \mu_i^{\text{L}} &= \mu_i^{\text{V}} = \mu_i^{\ominus}(\text{g}) + RT \ln p_i / p^{\ominus} \\ &= \mu_i^{\ominus}(\text{g}) + RT \ln p_i^* a_i / p^{\ominus} \\ &= \mu_i^{\ominus}(\text{g}) + RT \ln p_i^* / p^{\ominus} + RT \ln a_i \end{aligned}$$

$$\mu_i = \mu_i^* + RT \ln a_i$$

同理:

$$\begin{aligned}\mu_{\text{B}}^{\text{L}} &= \mu_{\text{B}}^{\text{V}} = \mu_{\text{B}}^{\ominus}(\text{g}) + RT \ln p_{\text{B}} / p^{\ominus} \\ &= \mu_{\text{B}}^{\ominus}(\text{g}) + RT \ln K_{\text{Hx,B}} a_{\text{x,B}} / p^{\ominus} \\ &= \mu_{\text{B}}^{\ominus}(\text{g}) + RT \ln K_{\text{Hx,B}} / p^{\ominus} + RT \ln a_{\text{x,B}}\end{aligned}$$

惯例 II 参考  
状态化学势

$$\mu_{\text{B}} = \mu_{\text{x,B}}^* + RT \ln a_{\text{x,B}}$$

## 讨论:

### 1. 活度可看成是一种校正浓度

$$p_i = p_i^* x_i \gamma_i = p_i^* a_i$$

$$\gamma_i > 1 \quad a_i > x_i \quad p_i > p_i^* x_i \quad \text{正偏差系统}$$

$$\gamma_i < 1 \quad a_i < x_i \quad p_i < p_i^* x_i \quad \text{负偏差系统}$$

$$x_A \rightarrow 1 \quad \lim_{x_A \rightarrow 1} \gamma_A = 1$$

$$x_B \rightarrow 0 \quad \lim_{x_A \rightarrow 1} \gamma_{x,B} = 1$$

理想稀溶液

讨论:

## 2. 活度与逸度的关系

$$p_i = p_i^* x_i \gamma_i = p_i^* a_i$$

$$f_i = f_i^* x_i \gamma_i = f_i^* a_i$$

$$a_i = \frac{f_i}{f_i^*} \quad \gamma_i = \frac{f_i}{f_i^* x_i} \quad \text{—— 相对逸度}$$

讨论:

### 3. 活度的数值取决于参考状态的选择

$$\mu_i = \mu_i^* + RT \ln a_i = \mu_{x,i}^* + RT \ln a_{x,i}$$

$$a_i \stackrel{\text{def}}{=} \exp \frac{\mu_i - \mu_i^*}{RT} = \frac{\lambda_i}{\lambda_i^*}$$

活度( $a$ )的定义

讨论:

### 3. 活度的数值取决于参考状态的选择

$$\mu_i = \mu_i^* + RT \ln a_i = \mu_{x,i}^* + RT \ln a_{x,i}$$

$$a_i \stackrel{\text{def}}{=} \exp \frac{\mu_i - \mu_i^*}{RT} = \frac{\lambda_i}{\lambda_i^*}$$

$$\gamma_i \stackrel{\text{def}}{=} \frac{a_i}{x_i}$$

活度因子的定义

讨论:

4. 活度因子的计算——由实验数据计算:

$$py_i = p_i^* x_i \gamma_i$$

$$py_i = K_{Hx,i} x_i \gamma_i$$

$$a_i = \frac{p_i}{p_i^*} = \frac{py_i}{p_i^*} \quad \gamma_i = \frac{p_i}{p_i^* x_i} = \frac{py_i}{p_i^* x_i}$$

活度因子关联式:

范拉方程

$$\ln \gamma_i = A_{12} \left( \frac{A_{21} x_2}{A_{12} x_1 + A_{21} x_2} \right)^2$$

威尔逊方程

$$\ln \gamma_i = 1 - \ln \sum_{j=1}^K \Lambda_{ji} x_j - \sum_{j=1}^K \left( \frac{\Lambda_{ij} x_j}{\sum_{k=1}^K \Lambda_{kj} x_k} \right)$$

## 4. 其它惯例参考状态——惯例III

$$p_B = K_{Hb,B} b_B$$

$$\mu_B^V = \mu_B^\ominus(\text{g}) + RT \ln \frac{K_{Hb,B} b^\ominus}{p^\ominus} + RT \ln \frac{b_B}{b^\ominus}$$

惯例III参  
考状态  $\mu_{b,B}^{**}$

系统温度压力下单位  
质量摩尔浓度的理想  
稀溶液溶质的化学势

$$\mu_B = \mu_{b,B}^{**} + RT \ln \frac{b_B}{b^\ominus}$$

## 4. 其它惯例参考状态——惯例IV

$$p_B = K_{Hc,B} c_B$$

$$\mu_B^V = \mu_B^\ominus(g) + RT \ln \frac{K_{Hc,B} c^\ominus}{p^\ominus} + RT \ln \frac{c_B}{c^\ominus}$$

惯例IV参  
考状态  $\mu_{c,B}^{**}$

系统温度压力下单位  
体积摩尔浓度的理想  
稀溶液溶质的化学势

$$\mu_B = \mu_{c,B}^{**} + RT \ln \frac{c_B}{c^\ominus}$$

## 5. 不同惯例(参考状态)间活度因子的换算

$$\begin{aligned} p_B^* x_B \gamma_B &= K_{Hx,B} x_B \gamma_{x,B} \\ &= K_{Hb,B} b_B \gamma_{b,B} \\ &= K_{Hc,B} c_B \gamma_{c,B} \end{aligned}$$

## 6. 渗透因子

表3-2 25°C, 101325Pa下蔗糖 $C_{12}H_{22}O_{11}(B)$ 在水 $H_2O(B)$ 中的活度因子

$x_A$	$\gamma_A$	$\gamma_{x,B}$	$\gamma_{b,B}$	$\gamma_{c,B}$	$\phi_A$
0.995	0.9999	1.047	1.042	1.103	1.020
0.980	0.998	1.23	1.21	1.50	1.099
0.960	0.990	1.58	1.51	2.26	1.246
0.930	0.968	2.31	2.15	4.07	1.448
0.900	0.939	3.23	2.91	6.78	1.597

$$\phi_A \stackrel{\text{def}}{=} \frac{\mu_A - \mu_A^*}{RT \ln x_A} = \frac{\ln(x_A \gamma_A)}{\ln x_A}$$

## 7. 标准状态和参考状态的关系

### 热力学标准状态

气体、液体、固体

### 逸度的参考状态(标准状态)

气体、液体、固体

### 活度的参考状态

溶剂、溶质